

Recent Progress in Doped TiO₂ Photocatalysis and Hybrid Advanced Oxidation Processes for Organic Pollutant Removal from Wastewater

DARSHANA TUSHAR BHATTI^{1*} and SACHIN PRAKASH BHAI PARIKH²

¹Chemical Engineering Department, Vvp Engineering College Affiliated to Gujarat Technological University, Rajkot, Gujarat, India.

²Directorate of Technical Education, Gandhinagar, Gujarat, India.

Abstract

Hybrid advanced oxidation processes (HAPOs) for the removal of non-biodegradable organics from wastewater have been studied in recent literature. With the increase in industrial development, the quantity of wastewater generated from these industries also organic wastewater produced by industrial manufacturing has posed threats to the environment. AOP's are one of the promising advanced technologies for mineralization of organics present in wastewater. Hybrid advanced oxidation process based on the ozonation, sonolysis, Photo-Fenton reagents and electro chemical method, has greater potential for complete mineralization of recalcitrant organics. This review article includes recent progress in the research and application of TiO₂ photocatalysis for the removal of non biodegradable organic pollutants present in water. It will provide a quick reference for various hybrid AOPs systems and their effectiveness. This review article provides quick insights into (1) hybrid AOP for treatment of various industrial effluents or model effluents, (2) work done on doped/co-doped photo catalyst as heterogeneous catalysts (3) study of parameters affecting the photocatalysis to enhance complete oxidation of organics present in wastewater. A mechanistic investigation of hybrid advanced oxidation processes with combinations of sonolysis and Fenton process coupled with UV, adsorption and addition of biochar has been discussed.



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Hybrid Aop Systems;
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Introduction


Innovations and productions of new medicines increased number of pharmaceutical industries

with accumulation of waste in rivers and on land. Environmental management part always found non-focused and lead to degradation of nature.

CONTACT Darshana Tushar Bhatti ✉ darshana333@gmail.com 📍 Chemical Engineering Department, Vvp Engineering College Affiliated to Gujarat Technological University, Rajkot, Gujarat, India..



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Researchers are working on these issues to resolve these problems. This situation enforced research towards zero effluent discharge, green technology and cleaner development mechanism. Semiconductor photocatalysis has been extensively studied by many researchers for the complete oxidation of refractory organics present in effluent,¹⁻³ water splitting for hydrogen production⁴ and solar cells.⁵ The application of TiO₂ as a photocatalyst is limited by UV radiations and recombination of the hole and electron pairs.^{6,7} Rapid industrialization has vastly increased water and air pollution problems as the current generation are interested more in profit and less concerned about waste generation. This situation demands fruitful research be done on waste minimization to avoid such situations and to achieve sustainable development. Objective of this review is to search for efficient and cost-effective AOP for wastewater treatment. Solar light-driven effluent treatment methods have been focused and developed for research.⁸ Titanium dioxide is an N-type semiconductor having an oxygen deficit in its structure. TiO₂ is a superior, nontoxic stable and economical photocatalyst that provides a non-selective and efficient oxidizing agent, Hydroxyl radical (OH^{*}).^{9,10} TiO₂ has shown certain limitations as a photocatalyst: 1) it has a large band gap and works only under UV radiations; 2) its low quantum yield of OH^{*} due to recombination of holes.¹¹

Metal doping in TiO₂ improves its absorbance in the visible region, e.g. a Ag: 300-800 nm, Co: 400-650 nm and Fe: 300-800 nm,¹²⁻¹⁴ and allow it to work under solar radiation to make cost-effective treatment.; 2) provides the excellent trap of electrons prevents recombination of e⁻ and holes results in superior photoactivity;¹⁵ 3) the Bandgap reduces from pure TiO₂ (3.1 eV) to doped TiO₂ (2.8 eV),^{16, 17} Silver and iron are extensively investigated as a dopant for TiO₂ and proved superior photocatalysts for mineralization of active pharmaceutical ingredients (API).¹⁸⁻²⁰ Co-doping of TiO₂ using metal dopants is a promising technology for solar mineralization of refractory organics in wastewater. Doping of TiO₂ with Fe and Ag metals enhances the photocatalytic activity due to large reactive sites for photocatalysis.²¹⁻²⁶ Nanomaterials have magical physical and ocular characteristics due to their size and in carceration e to initiate quantum properties. Nanopowder absorbs much more solar

radiation compared to nanofilms. Size, morphology and optical properties can be controlled during solar photocatalysis and photovoltaics results in better absorption of solar irradiations.^{27,28} Several studies on the photo activity of Ag-doped TiO₂ and Ag-Fe co-doped TiO₂ (Ag-Fe CT) catalyst proved co-doped catalyst superior over undoped TiO₂.^{25,29,30} Anisotropic structure of Ag dopant improved solar radiation absorbance.³¹ In this review, we have described recent progress in advanced oxidation processes with metal dopants, co-doped photocatalysts with their properties and bandgap. Synthesis of nano-doped TiO₂, mechanism of degradation by photocatalysis, operating variables and their effects on degradation and different techniques to modify optical properties of TiO₂ such as the use of metal and non-metal dopants, nanofilms, nanotubes and nanowires are discussed. The feasibility and the effectiveness of recycled photocatalyst have been studied. Hybrid AOPs is proved efficient compared to conventional AOP for complete mineralization of complex organics. Hybrid AOP using Fe doped TiO₂ has shown dual characteristics of photocatalysis and Fenton reaction, which has improved decolorization of wastewater.³² Photocatalytic treatment work under normal ambient conditions.³³ Efficient methylene blue degradation using combining AOP with Fenton reagents, results in production of more OH radicals.³⁴ Diclofenac and ibuprofen were converted efficiently in to biodegradable intermediates using planar falling film reactor and Coated TiO₂ on a Pilkington Active glass under UV radiations.^{35,36} This review will be useful to select efficient hybrid AOP for specific industrial wastewater treatment.

Advanced Oxidation Processes

AOPs are effluent treatment technology that produces a hydroxyl radical (OH) with highest oxidation potential and performs oxidation of organics to produce carbon dioxide and water as end products. These processes use ozone, photo Fenton reagents, hydrogen peroxide, or semiconductor photocatalysis to generate OH. TiO₂ was focused on photocatalysis by many researchers. It is available in three forms anatase, brookite and rutile. Amongst all these, the tetragonal anatase structure performs efficient photocatalysis.^{37,38} Various advanced oxidation processes consist of pollutant removal technologies

in which hydrogen radicals serve as an active medium. The methods are separated according to the source of the formation of hydroxyl radicals as shown in Fig. 1.³⁹

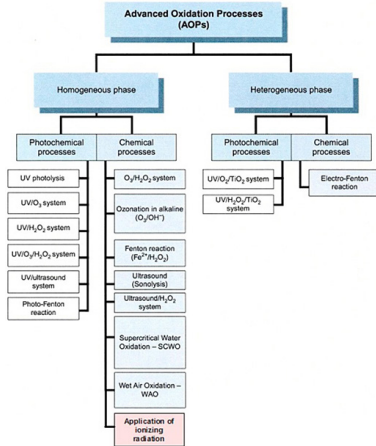


Fig. 1: Types of Advanced Oxidation Processes

Table 1 shows the oxidation potentials of various oxidizing agents. OH. Radical is nontoxic, nonselective and has the highest oxidation potential hence it is capable to mineralize a major category

of organic materials from wastewater during photocatalysis.

Table 1: Oxidation potential of different oxidants⁴⁰

Oxidizing Agent	Potential of oxidation (V)
OH•	2.8
O ₂ ⁻	2.4
O ₃	2.1
H ₂ O ₂	1.8
HOCl	1.5
O ₂	1.2

Some benefits of research of AOPs are as follows:

1. Newer technology to produce strong and non specific hydroxyl radical oxidizing agent;
2. To set up the highest standards for effluent treatment;
3. To develop an advanced mode of operation and competitiveness.

Table 2 summarizes different AOPs used for the degradation of various organics.

Table 2: Different Advanced Oxidation Processes for component degradation

Sr. No.	AOPs	Component for degradation	Experimental conditions	Results	Ref.
1	TiO ₂ -photocatalytic degradation	Tetracycline (TC)	Total Carbon 5–20 mg/L, TiO ₂ - 0.5-2 g/L 30 min in dark, 2 hr for photocatalytic degradation, TiO ₂ - 1 g/L, 12 W halogen lamp Total Carbon 10 mg/L	Optimum TiO ₂ conc.1 g/L Toxicity removal 84 % in 240 min	19
2	aerobic, anaerobic, aerobic/anaerobic reactor, sonication, photocatalysis reactor	Ciprofloxacin (CIP)	Aerobic/anaerobic sequential reactor system – Hydraulic retention time=10 days Organic loading rate= 0.2 g COD/L, Sonication at a power of 640 W and 35 kHz 45°C, pH 7, 45 min irradiation time, 210 W UV lamp, 0.5 g/L TiO ₂ 25°C	COD removal and CIP yields were 95% and 83%, 95% and 81% after 45 min, 98% and 88%	41
3	TiO ₂ -assisted ozonation in water	cyanotoxin cylindrospe-rmopsin (CYN)	pH 7, O ₃ 0.25-2 mg/L, TiO ₂ =500 mg/L, CYN 5 mg/L	Pseudo first order, ozonation increased degradation from 75.7% to 98.9%.	42

4	hybrid ozonation -nano filtration- continuous process	ozone – 1.17-4.85 mg/lit, NF module.- (AFC30) Polyamide film membrane with 75% CaCl ₂ retention, Flow rate: 8 L/min, 30 bar, 25°C	COD inlet 1300 mg/L COD outlet 50 mg/L (96.15 %) ozone treatment increase permeate flux and decreased fouling index due to less flocculation so pores are not clogged.	43	
5	Ozonation, H ₂ O ₂ /UV and TiO ₂ Photo- catalysis	Carbamazep -ine, propranolol, clofibrac acid, diclofenac, oflo -xacin, sulfamet -hoxazole, blue- green algae	Hydrogen peroxide (30% w/w), pH 7.6, time: 20 min, ozone 13.875 mg/L, 0.3 gm/L TiO ₂ , UV 300 W, 48hr	Complete removal of toxicity (% survival of blue-green algae Synechococcusleo -poliensis, rotifer), 80 % removal of each organic	44
6	Combined GAC adsorption and UV254/H ₂ O ₂	pharmaceutical wastewater	2.12 to 6.37 mg H ₂ O ₂ /mgCOD, time 3hr, pH 3.4 20-60 min GAC, pH 3.4	Highest TOC removal 88%	45

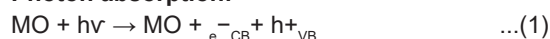
Major merits of AOP includes the faster rate of mineralization, non biodegradable organics are completely oxidized into CO₂ and H₂O, treated effluent can be directly reused without further purification, avoid sludge generation and its handling problems, it can be easily clubbed with existing ETP with little modification, and economic operation and maintenance compared to incineration. Demerits of AOPs are higher capital costs, complex and unknown reaction chemistry may sometimes lead to more hazardous intermediates formation and photochemical reactor design and operation are difficult. Challenges of AOPs are Photocatalyst deactivation and unknown routes for different reactions,⁴⁶ development of proper doped catalysts to enhance the absorption of solar radiation, the selectivity of photocatalyst may sometimes pose a problem in treatment when a mixture of different organics is present, electron and hole recombine to result in lower net generation of OH radicals, scale-up and commercialization of process⁴⁷ and UV radiations may sometimes degrade ozone, chlorine and hydrogen peroxide which are useful oxidizing agents in the process.³⁹

Titanium Dioxide Photocatalysis

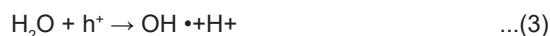
Semiconductor oxides have a greater number of

surface atoms on a surface which enables photon absorption and performs various oxidation and reduction reactions for complete removal of a variety of organics from aqueous solutions. Titanium dioxide is widely preferred for photocatalysis due to its stability, reusability, nontoxicity, anti-corrosiveness and low cost. Different other oxides that can also be used for photocatalysis are zinc, tin, zirconium, cadmium and iron. Hydroxyl radicals react with organics to produce carbon dioxide and water.^{6,48} The main reactions involved in photocatalysis are shown below (equation (1) to equation (8)):⁴⁹

Photon absorption:

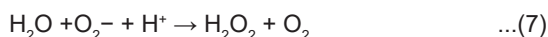


Oxidation:



Reduction:





Electron and hole combination:



where MO is a metal oxide, $h\nu$ are photons, h^+ are holes. When photons bombard on TiO_2 surface it enables electron movement and reactions on an interface where large numbers of organic substances are absorbed from the effluent. Semiconductor TiO_2 absorbs photons and transfer electron from the valance band (vb) to the conduction band (cb). On the valence band, holes are generated which reacts with H_2O or OH^- to produce hydroxyl radicals. TiO_2 is N-type semiconductor material. Hole performs oxidation reactions and electron performs reduction reactions as shown in equations (1) to (9) on the surface along with complete oxidation of organics to produce CO_2 and H_2O .

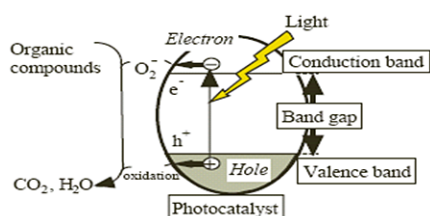


Fig. 2: Mechanism of photocatalysis⁵⁰

When semiconductors such as TiO_2 absorb light e^- jumps from the vb to the cb. Nanoparticles have a large surface to volume ratio and also contain more atoms on their surface which substantially absorb photons. Nanoparticles can perform photocatalysis rapidly before e^- and hole recombine.^{17,51} Parameters affecting photocatalysis are Organic load, catalyst concentration, reactor design (batch, continuous, immobilized/suspended catalyst etc.), adsorption and UV irradiation time (optimum), temperature, pH, light intensity and presence of ionic species.⁸¹

Doping in Nano-Structured TiO_2 for enhanced photocatalytic activity

Doping is one of the methods to improve optical properties, reduce bandgap and overcome e^- /hole recombination as metals trap e^- result in enhanced photocatalytic activity of semi conductor oxides. Doping will provide efficient and economical photocatalysis as it can replace UV photocatalysis with solar or visible irradiations. Loading of TiO_2 surface with dopant will engineer the photocatalyst

with improved trapping of charge carriers. Thus Doping increases organics degradation efficiency.⁵² Dopant will create oxygen defects and shifts light absorption from UV to the visible region by improving absorption bandwidth. The efficiency of photocatalysis may differ based on the position of the dopant on the TiO_2 structure. Based on synthesis methods, the dopant can take a position on the surface or it can be included in lattice structure or as core and thus these positions may lead to different photocatalytic activity and degradation efficiency. Metals and non-metals both can work as dopants but major research concludes that metal dopants possess strong surface plasmon resonance (SPR), work efficiently under solar radiations during photocatalysis.⁵³

For efficient photocatalysis, the bandgap should be lower which promotes the transfer of e^- and holes. This will also influence the redox potential of photogenerated electrons and the oxidation potential of holes.⁵³ The handling of TiO_2 powder form is difficult and the cost of UV radiation makes the treatment energy-intensive and uneconomical. These issues limit the commercialization of AOPs for industrial effluent treatment. These limitations can be overcome by surface modification of TiO_2 with transition metal doping which reduces the bandgap and greater absorption of visible light is possible, also the dopant metals trap e^- and prevent its recombination with holes, hence, the photocatalysis can be performed under solar radiation to make system economical for removal of refractory organics compared to incineration treatment. Various metal dopants are Chromium, manganese, cobalt, copper, iron, Nickel, Zinc, cerium, Neodymium, Europium, Lanthanum, etc. and various non-metal dopants are Palladium chloride, carbon, nitrogen, and Fluoride.

Recyclability of Photocatalyst

TiO_2 doped with 33% Fe_2O_3 core-shell photocatalyst has enhanced paracetamol removal by photocatalysis from water and the photocatalyst could be easily separated and reused for four recycle runs.²⁸ Ag decorated $\text{Fe}_3\text{O}_4/\text{TiO}_2$ coated cenosphere prepared via Modified sol-gel and wet impregnation can be recycled for 8 cycles with a slight reduction in Methylene blue degradation efficiency.²⁶ The novel engineered photocomposite core-shell structure $\text{Fe}_3\text{O}_4@\text{SiO}_2@\text{TiO}_2$ showed greater photoactivity

compared to commercial TiO_2 . The catalyst provided easy separability using a magnet and was recycled for 10 numbers of recycling runs without a decrease in efficiency.²² When the Ag-Fe CT with Ti/Ag mole ratio 30 photocatalysts were reused for six numbers of runs, 63.25% COD was removed in 5 hr solar light irradiation, indicating more deactivation of the catalyst during photocatalysis; which represented that the Ag-Fe CT 30 could be recyclable effectively for 4 cycles. The reduction in % COD removal was only less than 5% after three runs of recycling for Ag-Fe CT 30. Ag-Fe CT 30 catalyst has proved its stability even after 4 recycle runs and it can perform photocatalysis under solar radiation effectively for the photocatalysis of drug intermediates.¹⁶

Dye degradation efficiency by Fe^{3+} doped TiO_2 has been found to decrease by 9% at the end of six recycle runs.⁵⁵ Ag-Fe CT and $\text{Fe}_2\text{O}_3/\text{SiO}_2$ co-doped TiO_2 and Ag-Fe CT supported on graphene oxide has shown good stability for 5 recycle runs.⁵⁸ Table 4 summarizes the literature review done for the recyclability of photocatalysts. The photocatalysts can be recovered after treatment and efficiently used for several runs without loss in efficiency of treatment or component degradation. The result showed a decrease in photocatalytic activity with an increase in the number of recycling runs as the poisoning of the catalyst increases due to surface blockage, less adsorption and low rate of oxidation reaction.⁷

Table 3: Feasibility and effectiveness of photocatalyst for recyclability

Sr. No.	Catalyst	Synthesis method	Model pollutant and expt. Conditions	Recyclability runs	Result	Ref.
1	$\text{Fe}_3\text{O}_4\text{-TiO}_2$	Solvothermal and micro-thermal method	Phenol, UV light, 100-300 min, 0.5 g/L	2	Degradation was 100%, 70%, 32% for P25 and $\text{Fe}_3\text{O}_4\text{-TiO}_2$ (3 ml titanium butoxide), $\text{Fe}_3\text{O}_4\text{-TiO}_2$ (10 ml Titanium butoxide) respectively	2
2	$\text{Fe}_3\text{O}_4@\text{SiO}_2/\beta\text{-NaY F4:Yb}^{3+}, \text{Tm}^{3+}/\text{TiO}_2$	sol-gel process and solvothermal	methylene blue, methyl orange, rhodamine B, and phenol under, 1-10 ppm, 144 min, Laser light, 10 g/L	4	76.62%, 68.48%, 30.05% and 27.16%	57
3	Ag-doped TiO_2 , Ag:Ti molar ratio: 0.02-0.12	solgel	Acetamidiprid- 20 mg/L-insecticide, UV light, 60 min, 0.4 g/L	6	Ag/Ti = 0.06 opti, as Ag increase rutile phase increase	58
4	Fe^{3+} -doped TiO_2 -1-4 wt %	modified sol-gel	azo dye acid orange 7-50 mg/L, solar, UV and visible light, 18 min, 0.3 g/L	4	100 % UV, 100 % visible, 90 % solar in 2 hr, 3 wt % opt-98.9 %	55
5	N- $\text{TiO}_2/\text{Fe}_3\text{O}_4 @\text{SiO}_2$ and Ag-Fe	coprecipitation	bisphenol A: 2 mg/L, visible light, 90 min	3	100 % and 88% using Ag-Fe and N- $\text{TiO}_2/\text{Fe}_3\text{O}_4 @\text{SiO}_2$ respectively	56
6	Ag-doped TiO_2 -P25	surface impreg	Drug: pentoxifylline	10	Ag- TiO_2 -P25: Opt.: 0.75 g/L cat	30

	supported on Clay beads, Fe-Ag-TiO ₂ composite (1.5 wt %)	-nation method	(PEN) 50 mg/L, 40 ml solution, solar, 1.5 g/L, 30 min		conc., 75% and 68% degradation in TOC and COD resp. 90% degradation of PEN in 30 min	
7	graphene oxide supported Ag-Fe TiO ₂ -1 wt% of Ag	chemical reduction and the hydro thermal	methylene blue 20 mg/L and 4-NP, visible, 150 min, 0.2 g/L	3	rGO supported Ag-Fe CT, rGO supported Fe -TiO ₂ , Fe -TiO ₂ and undoped TiO ₂ -95 and 89%, 82%, and 74.6%, respectively	29
8	Clay suppo. Fe doped TiO ₂ (1-4 %: 2% opt)	surface impregnation method	Pesticide- Carbendazim: 4-10 gm/L, UV and solar, 4 g/50 clay beads, 300 min	40	70 % degrade-UV. TiO ₂ : 82 UV+63 sun light, Fe TiO ₂ - 93 % sun light and 67 % UV	59
9	Fe ³⁺ doped TiO ₂ film- with Fe ³⁺ =0, 1, 3, 5, 7 and 10	spin coating	methylene blue, 5 mg/L, 25 mL, visible, 240 min	10	96.7 % at 7% opt. 83.5 % at 10th round end	60
10	Fe doped TiO ₂ -3%	Sol gel	methylene blue: 10-5 mg/L visible, 150 min, 0.5 g/L		59, 97, 79 % for TiO ₂ , 3% Fe and 7% Fe-TiO ₂	7
11	Cu ²⁺ , Ag ⁺ , Zn ²⁺ , Fe ³⁺ , and Al ³⁺ ion and Pt metallic +effect of doping, Cr ³⁺ , Mn ²⁺ and Co ²⁺ : -ve effect of doping	Sol gel, 0.5 mol % dopant metal	Para nitrophenol: 10-4 mol/L, 480 min, 1 g/L	3	50 % -TiO ₂ , 55: Fe 0.5, Fe 2 : 35, Fe 5: 15, Ag 0.5: 58, Ag 2: 60, Pt 0.1: 79 %	61
12	Ag-doped TiO ₂ pillars-2.8 %	Wet impregnation and high temp thermal reduction	2,4-dichlorophenol -5 mg/L-30 ml, visible, 120 min 1.67 g/L	10	99 %	62
13	Au-Ag NPs -decorated TiO ₂ -modified Fe ₃ O ₄	Solvo thermal	Textile waste water- Rh6G dye 30 ppm, xenon lamp, 60 min 2.67 g/L	5	95 % removal. 8% efficiency decreased after 5 runs	38

*NA: data not available

Ammonical nitrogen removal using photocatalysis

NH₄-N removal is higher in alkaline pH during photocatalysis. At lower pH, the surface of photocatalyst has a positive charge whereas

ammoniacal nitrogen compounds can be adsorbed only on the surface which has a negative charge.⁹³ NH₄-N removal is more when pH is greater than 10. Researchers have reported that it is not possible to oxidize NH₄-N OH by radicals.⁹⁴

When pH is above 9, $\text{NH}_4\text{-N}$ can be converted into NH_3 .⁹⁵ Hence acidic or neutral condition does not favor $\text{NH}_3\text{-N}$ removal simultaneously

with organics. Table 5 summaries research done for ammonical nitrogen removal by photocatalysis.

Table 4: Ammonical nitrogen removal during photocatalysis

Sr. No.	Catalyst	Synthesis method	Model	light pollutant	Opt pH	Catalyst	Time, dose	Result hr	Ref.
1	TiO_2 film on glass beads: to 10 layers of TiO_2 thin film.	Coating with sol-gel method	NH_4Cl solution 300 ml, ammonia conc. 700 mg/L	UV light	7	film	2 hr	6 coating opt, 70 % removal efficiency	66
2	Cu/ZnO/rGO Nanocomposite	Sol-gel	Domestic wastewater $\text{NH}_4\text{-N}$: 10, 30, 50, 70, and 100 mg/L	Visible-Xenon lamp	10	0.2-2 g/L, opt 2	2 hr	Optimum : $\text{NH}_4\text{+con.}$ = 50 mg/L, catalyst conc. = 2 g/L, pH 10. 83% removal efficiency	67
3	La/Fe/ TiO_2 composite	Sol-gel	NA	500 W mercury lamp	10	1 g/L,	3 hr	64.6% removal efficiency	68
4	TiO_2	Sol-gel	Secondary treated effluent: Ammonia conc. 26 – 214 mg/l	UV light	10.7	2.1 g/L	3.5 hr	50 % removal efficiency	65
5	Ag/ Fe co-doped TiO_2	Sol-gel	Industrial effluent, COD: 88660 mg/L, $\text{NH}_3\text{-N}$: 3287 mg/L	Solar	5	1g/L	5 hr	64.69% COD removal, 16.05% $\text{NH}_3\text{-N}$ removal	16

*NA: data not available

Hybrid Advanced Oxidation processes

COD removal using three methods, combining electrochemical process with AOP, Fenton reagent and flotation HAOP technology has been proved effective in the treatment of pharmaceutical wastewater for COD removal⁶⁹. An ultrasound when used in combination with photocatalysis, Fenton Reagent and the Photolysis process, proved efficient for non-biodegradable toxic organics removal. This combination of AOP will overcome problems of repelling photocatalyst and pollutants due to similar charges. A sonophotocatalysis has been found effective for the removal of variety

of organics present in wastewater.⁷⁰ Hybrid AOPs with sonolysis, Fenton and photo-ferrioxalate system with sonolysis has been studied for degradation of two dyes: Acid Red B and Methylene Blue. Sonolysis alone has shown the lowest efficiency. Coupling of sonolysis with either Fenton or photo-ferrioxalate system has shown the greater ability of decolorization. Ternary coupling of all these three systems has shown a negative effect of dyes degradation due to the interaction of individual mechanisms⁷¹. Table 5 summaries research done on hybrid advanced oxidation processes.

Table 5: Hybrid advanced oxidation processes

Sr. No.	Hybrid AOP	Compound for degradation/treatment	Experimental condition	Result	Ref.
1	Advanced oxidation with O ₃ addition, adsorption by activated charcoal	Pharmaceutical effluent	pH 5-11,, time – AOP- 3 hr, adsorption with charcoal - 2.5 hr	H2O2 addition with AOP: COD removal: 75-88%. Further continuation of treatment with adsorption by activated charcoal- COD removal reached up to 93%	72
2	hydrodynamic cavitation with Fe ₃ O ₄ nanophoto-catalyst	P-nitrophenol (PNP)	8 atm -pressure, 3-pH, 20 mg/L- PNP, Fe ₃ O ₄ to H ₂ O ₂ ratio= 1:1, H ₂ O ₂ :0.6 mol/L,	PNP degradation 78%	73
3	hydrodynamic cavitation (HC) with ZnO/ZnFe ₂ O ₄ and persulfate system+ Magnetic separation for recycle	Carbamazepine (CBZ)	9 atm-pressure, 4-pH, 15 mg/L-CRZ, 18 W UV, 500mg/L- Na ₂ S ₂ O ₈ , 500 mg/L- ZnO/ZnFe ₂ O ₄	98 % CBZ degradation	74
4	electrocatalytic process	Industrial raw effluent (antibiotics)	Cathod: carbon, anode: Ti/PtIr plate	100% COD removal	33
5	UV/ZnO nps/O ₃	4-Nitro aniline (4-NA)	catalyst dose: 3 g/L, pH:5, 4-NA: 10 mg/L, time: 60 min	Degradation of 4-NA: 92%	75
6	MOFs@COFs hybrid materials with C ₃ N ₄ : sulfate radical-based advanced oxidation processes	bisphenol A (BPA)	Visible light	BPA degradation 99%	76
7	UV-C or hydrogen peroxide	Boscalid, pyra-clostrobin, fenbuconazole and glyphosate- Pesticides removal on apple dyes	H ₂ O ₂ , UV-C	glyphosate -99% removal, boscalid, pyraclostrobin and fenbuconazole degradation 88 %, 100 % and 70 % respectively	77
8	CuO particle-WO ₃ nanofiber hybrids-(adsorb-ent/photocatalyst)	dyes	WO ₃ nanofibers and CuO nps, visible light	dyes removal-90%, 0.75 wt.% CuO adsorbed 38% higher and degraded 26% more methylene blue than WO ₃ nanofibers	78

9	hybrid photocatalysis and Cr(III) dispersed membrane-geo polymer membrane separation	Dyes wastewater	50 min at 0.09 MPa	100% degradation	79
10	nano-sheet C ₃ N ₄ -WO ₃ composite (nsCW21 with the addition of H ₂ O ₂)	Natural organic matter (NOM)	5 hr, visible light photocatalysis	Without the addition of H ₂ O ₂ : 71% removal, With the addition of H ₂ O ₂ : 91% removal, catalyst was stable up to 5 recycle runs.	80
11	Hybrid biochar-TiO ₂	textile wastewater treatment	74.3 mg/g, biochar (30.4 mg/g) and pure TiO ₂ (1.50 mg/g)	biochar and TiO ₂ alone - 85 % and 43 % degradation efficiencies respectively, coupling both-99% photo degradation efficiency	81

Conclusion

This review described various advanced oxidation processes with their merits, demerits, benefits and challenges. Various dopants have been compared for their enhanced photoactivity. The mechanism TiO₂ semiconductor doped with Ag and Fe has been discussed. The degradation of various chemical compounds using TiO₂-based photocatalysts, including mechanisms and factors affecting the process have been summarized. Hybrid AOP with photocatalyst is proved an effective method for treatment of wastewater. Addition of different oxidizing agent and materials such as H₂O₂, Fenton reagents and biochar have increased organics removal efficiency from wastewater. Electro Fenton and electrolysis, cavitation was used effectively for wastewater treatment. Advanced oxidation with O₃ addition, adsorption by activated charcoal for pharmaceutical wastewater treatment was also

effective. This paper concludes that proper selection of Hybrid AOP can provide efficient mineralization of organics present in wastewater at low cost. Recyclability studies showed that photocatalyst can be separated after treatment and reused up to several runs efficiently without much decline in treatment efficiency.

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Conflict of interest

The authors do not have any conflict of interest.

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