

## Hydraulic Design of Sewage Treatment Plant for Junagadh Agricultural University Campus

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### Abstract

The Junagadh Agricultural University campus is located in Junagadh, which lies in western Gujarat. The human population on the campus is multiplied distinctively due to the establishment of new schools and hostels. The university campus had a population of 1418 in the year 2013 when the supply of water was 152 lit/day per person and the sewage generation was 0.0084 m<sup>3</sup>/s (725.76 m<sup>3</sup>/day). Hence, a sewage treatment plant (STP) with suitable capacity is needed to deal with the elevated sewage. The recycled water can be utilized for agricultural purposes. This paper discusses about the design of STP and its major components such as skimming, grit chamber, and screening chamber, active sludge, sedimentation tank and secondary clarifier in the end sludge drying beds. The proposed design is suitable for 0.0672 m<sup>3</sup>/s sewage and would help to provide 58 MLD process capacity. In the end, treated water will have been used for irrigation purpose in the research field of a university.



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### Introduction

Water is one of the important and precious natural resources. Efficient use of water is important for agricultural production. At present, the use of chemical fertilizers in agriculture is increasing day by day but, the production of chemical fertilizers is

lesser than its demand. Moreover, treated sewage water is rich both in organic matter and nutrients which fulfil the requirement of plants (particularly phosphorus and potash). It can be profitably utilized either as irrigation water or as a manure to supply nutrients to different crops.<sup>1</sup>

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Sewage treatment is the procedure of disposing of contaminants, suspended solids from sewer water and domestic sewage, this material is sullied with several harmful natural and inorganic mixes.<sup>2</sup> It is a complicated combination of biological and physiochemical processes for removing physiochemical and biological unwanted contaminants. Which can be cleaned by the STP. The STP's main function is to recycle effluent and the solid waste or sludge to a reasonable level of quality for release or reuse once again into nature.

It is estimated that about 38,254 million litres per day (mld) of wastewater is generated in urban area class I towns and class II cities having a population of extra than 50,000 (accounting for more than 70 percent of the total urban population). The municipal

wastewater treatment capacity developed up to now is about 11,787 mld, that is approximately 31% of wastewater generated in class I & II towns. The status of wastewater generation and capacity of sewage treatment plant developed over past ten years in urban Areas (Class I & II) is shown in Table 1. On the basis of population growth in this country. The Requirement of freshwater for all users will become out of control. It's far estimated that the projected wastewater from the urban area may also pass 1,20,000 MLD via 2051 and that rural India will even generate not less than 50,000 MLD on the basis of water supply designs for community components in rural regions (see table 2). However, control plans of wastewater do no longer deal with this increasing pace of wastewater era.<sup>9</sup>

**Table 1: Generation and Treatment of sewage Capacity in Urban Centres<sup>3</sup>**

Parameters	Class I cities					Class II towns				
	1978	1989	1994	2003	2009	1978	1989	1994	2003	2009
	-9	-90	-5	-4		-9	-90	-5	-4	
Number	142	212	299	423	423	190	241	345	498	498
Population (millions)	60	102	128	187	187	12.8	20.7	23.6	37.5	37.5
Water Supply (mld)	8638	15,191	20,607	29,782	44,448	1533	1622	1936	3035	3371
Wastewater Generated (mld)	7007	12,145	16,662	23,826	35,558	1226	1280	1650	2428	2696
Wastewater treated (mld) (percent)	2756	2485	4037	6955	11,553	67	27	62	89	234
Wastewater untreated (mld) (percent)	4251	9660	12,625	16,871	24,004	1160	1252	1588	2339	2463

**Table 2: Generation sewage from urban areas and Projections for 2051<sup>3</sup>**

Year	Urban population (million)	sewage generation (lpcd)	Gross sewage generation MLD
1977-1978	72.8	116	7007
1989-1990	122.7	119	12145
1994-1995	151.6	130	16662
2003-2004	243.5	121	26254
2009	316.15	121	38254
2051	1000	121	120000

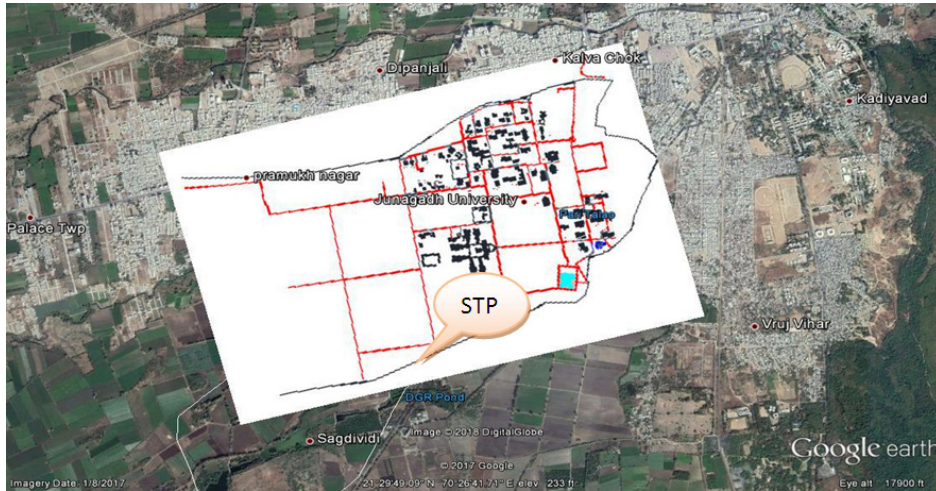


Fig. 1 The Proposed site for STP

Sewage suggests to a collection of sewage water from involved regions and transfers them to some point where it can dispose (at present there is no such conveying system exist within the campus area, which is required to be established). The fluid squanders would require remedy earlier than they're released into the water frame or in any other case disposed of without any harmful effect on peoples fitness or inflicting offensive conditions.<sup>6</sup>

In JAU campus present population is 1418 (with student and staff) by population forecasting method in 2042 population is 1888. Water supply to each person is 152 lit/day and sewage generation is 80% of water supply.<sup>3</sup> As per calculation sewage discharge is 0.0084m<sup>3</sup>/s. This is not feasible as per cost and design. To run the plant for 24 hr with this discharge is not possible. So, the plant is needed more discharge. That means one receiver chamber is required for collecting 24 hr sewage discharge in that way plant is run in two shifts of 1.5 hr in a day.<sup>7</sup> Proposal site for STP in JAU has shown in fig.1.

**Materials and Methods**

**Location of Sewage Treatment Plant (STP)**

Sewage treatment plant must be placed as near the land at such an area from wherein the dealt with sewage can immediately go with the flow under gravitational force closer to the disposal factor. The plant has to no longer be plenty a long way far from

the sewage starting place to lessen the length of the sewer line.

**Design**

Sewerage treatment plant has also the external part which includes underground sewer pipes and builds STP treatment component, which can't be easily changed or accelerated in their capacities without difficulty or quite simply in near future. For avoided such condition in the future expansions of the campus and as well as expansion within the sewage, amount ought to be forecasted to serve JAU satisfactorily for an affordable time. For the concern of future, some extra freeboard has provided in design so in next 30 year its component also work

Table 3: Test Report of sewage water samples of JAU Campus

PARAMETERS	RAW SEWAGE OF JAU campus	EFFLUENT (expected)
pH	7.33	5.5-9.0
BOD	106.87	≤ 20 ppm
COD	100.26	≤ 250 ppm
Oil and Grease	NA.	≤ 5 ppm
TSS	33.04	≤ 30 ppm
Nitrogen	NA.	≤ 5 ppm
Ammonical Nitrogen	NA.	≤ 50 ppm
Phosphorus (as PO <sub>4</sub> )	NA.	≤ 5 ppm
Total Coli form	5.29 x 10 <sup>6</sup>	≤ 1000 no/100 ml

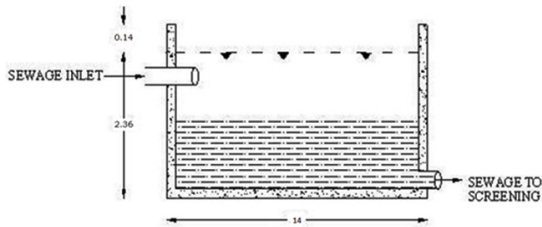


Fig. 2: Receiving chamber<sup>8</sup>

properly. Effluent realised from campus must meet the countrywide standards for wastewater set by Government authorities. So, Sewage Treatment Plant (STP) must design & operated in one of this manner that it treats the wastewater to those requirements.

**Calculation of Total Volume Sewage Generation**

Design period consider 30 years lifespan.  
 Present population in 2012 =1418  
 Forecasted population at 2042 =1888  
 Water Supply Per Capita = 152 l/day  
 Avg. water supply per day = 1888 x 152  
 = 286976  
 = 0.28 MLD

Avg. sewage generation per day is nearly 80% of supplied water.

$$= 0.8 * 0.28$$

$$= 0.224 \text{ MLD}$$

In cumec,

$$\text{Avg. sewage generation in a day} = \frac{0.224 \times 10^6}{1000 \times 24 \times 60 \times 60}$$

Avg. Discharge = 0.002824cumec  
 Maximum Discharge = 3 \* avg. discharge  
 = 3 \* 0.0028  
 = 0.008472cumec

**Points Considered for Design**

Following points are taken into consideration throughout the layout of STP:

- The design period has taken 30 years.
- The Design was not done by an hourly flow of sewage generated. But it will consider all year avg, daily flow of sewage.
- Rather than providing one high capacity component for every treatment more than two numbers small one to be provided, with a purpose to provide in operation in addition for

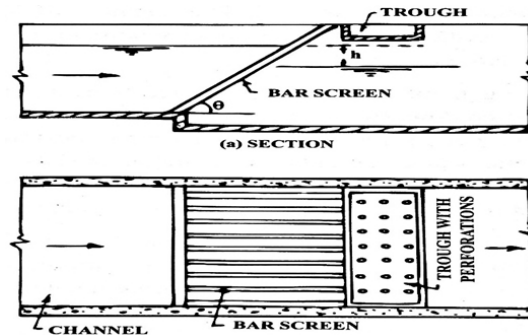


Fig. 3: Screen Chamber<sup>8</sup>

the plant will not stop at upkeep and restore time.

- For bypasses and Overflow, assembly should be kept in mind when designing every part.
- Self-cleansing speed of flow must create by design at each part in STP.
- The design of the STP parts should be economical, maintenance free and flexible for an uncertain condition.

**Design of Receiving Chamber**

It is an oblong form tank made at the doorway of the STP. The main pipe which is pass sewage is directly passed sewage to this tank.

Volume required = detention time X flow<sup>(4)</sup>

Area = Volume / depth

**Screening**

In this part row, sewage pass through different types of the screen on the way to catch and removed off the floating matter together with tree leaves, fiber, rags, timber pieces, paper, gravel, tampons, and kitchen refuse and many others.

**Design of Coarse screens**

It includes metallic rods which is placed at 30° to 60° angle to the horizontal axis. Space between rods is 50 mm or more. These gang of the rod is located inside the screen chamber at flow line of sewage.

The net area screen opening required = (Peak discharge of sewage )/0.25<sup>(4)</sup>

Clear area = 0.268 / 1 sin 60

**Design of Grit Chamber**

Grit removal chamber is working on sedimentation principal. Which has placed in front of the fine screen. When the flow has pass through it will have removed inorganic particles having Sp.gravity of 2.65. The grit chamber designed like that which catches the lighter organic matter at simultaneously and heavier organic matter remains in settled position.

Aerated volume= Peak flow of sewage x detention period<sup>(4)</sup>

Length of the channel = Aerated volume / Area

**Design of Fine Screen**

Fine screens are the filtering system which is placed between grit chambers and primary sedimentation

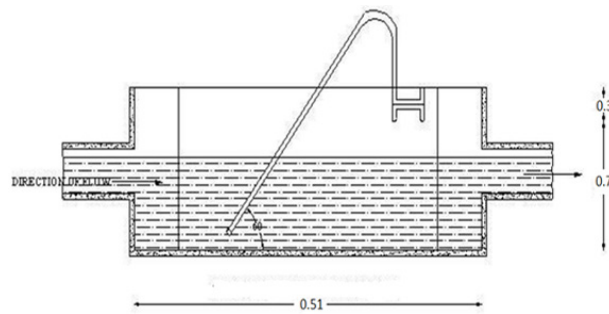


Fig. 4: Coarse screen<sup>8</sup>

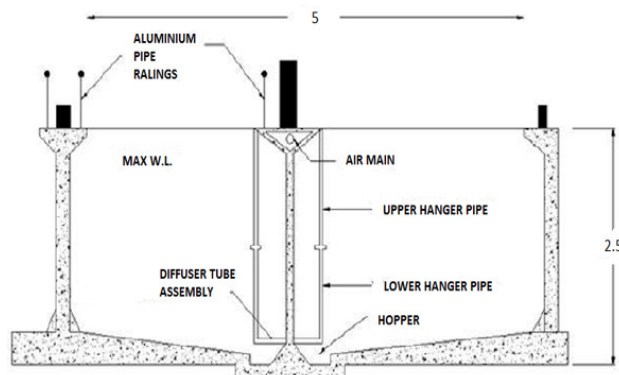


Fig. 5: Aerated grit channel<sup>8</sup>

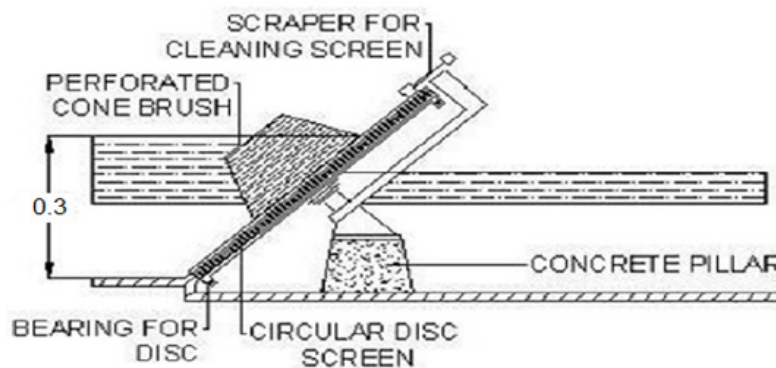


Fig. 6: Fine Screen<sup>8</sup>

tank which will take away a few quantities of suspended solids from sewage.

Width of channel = gross area / depth<sup>(4)</sup>

No of bar = Width of channel / thickness of bar + clear opening

**Design of Skimming Tank**

Skimming tanks are the tanks getting rid of oily material from the sewage built earlier than the sedimentation tanks. In skimming tank, air flow entering from the side and chlorine gas with the aid of air diffuser positioned from the bottom of the tank. Because of air rise tends to solidify and coagulate the grease and motive it to upward push to the top of the tank whereas chlorine gasoline destroys the protective combination impact of macromolecule that holds the grease in mixed form.

Required surface area of the tank A=

$$\frac{6.22 \times 10^{-3} \times q}{V_r} \text{ m}^2$$

Where,

V<sub>r</sub>= Min. rising velocity of the oily material to be removed in m/min

q= sewage flow rate in m<sup>3</sup>/day

**Design of Primary sedimentation tank**

Primary sedimentation tank is working like settling of heavy mater so that it is called a settling tank. Which was placed after skimming tank so that eliminate the natural solids that are too heavy to be removed i.e. the debris having sizelover then 0.2 mm and Sp.G of 2.65 and also built inclined plate clarification, those by use of gravityclarifiers work alongside the projected settling region as a manner to have an impact on a fairly immoderate

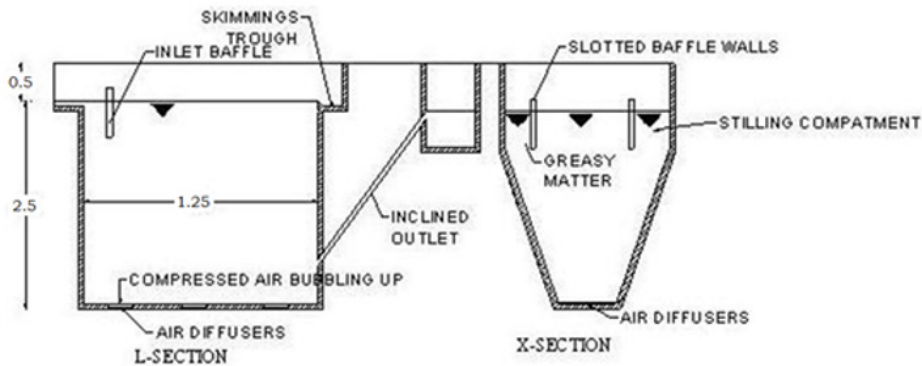


Fig. 7: Skimming Tank<sup>8</sup>

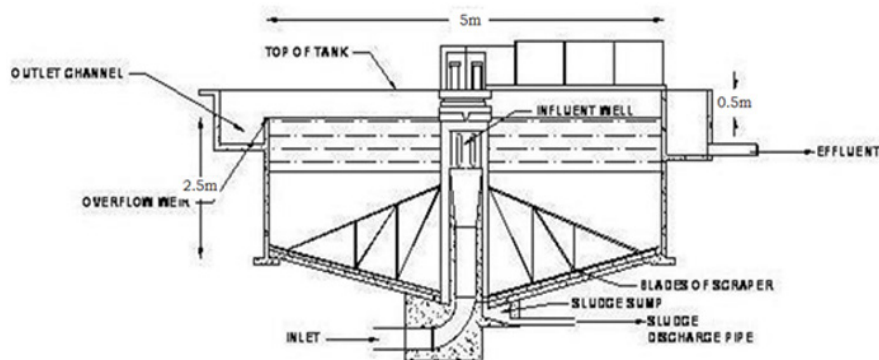


Fig. 8: Sedimentation Tank<sup>8</sup>

percentage of elimination of suspended solids as 60 to 65% of total TSS and 30 to 35% of the BOD from the Raw sewage.

Volume the tank = Hydraulic detention period x 2 / 24

$$\text{Volume of sewage} = \frac{\text{Quantity sewage} \times \text{Detention period}}{24} \text{ (4)}$$

Area = Volume / depth ,

$$\text{Surface Area the tank} = \frac{\text{Total flow}}{\text{Surface loading}} \text{ (4)}$$

Surface area = Average flow / Surface loading rate of flow (4)

$$\text{Diameter of the tank} = \sqrt{\frac{\text{Surface Area} \times 4}{\pi}} \text{ (4)}$$

$$\text{Diameter} = \sqrt{\frac{\text{Surface area} \times 4}{\pi}} \text{ (4)}$$

**Design of Secondary sedimentation tank**

Secondary sedimentation tank place at after aeration tank it's far known as secondary sedimentation. This tank is wished because of the number one sedimentation tank with high-quality adjustments as no floating substances are right here, provisions for the elimination of scum, floatage aren't desired.<sup>5</sup>

**Design of Sludge drying beds**

In this Drying processes of semi solid digested sludge on open-air beds on the land is call sludge drying and such system of open beds drying is call sludge drying beds. Moisture contains semi solid digested sludge is high which is comes from digestion tank. So it is required to dehydrate the

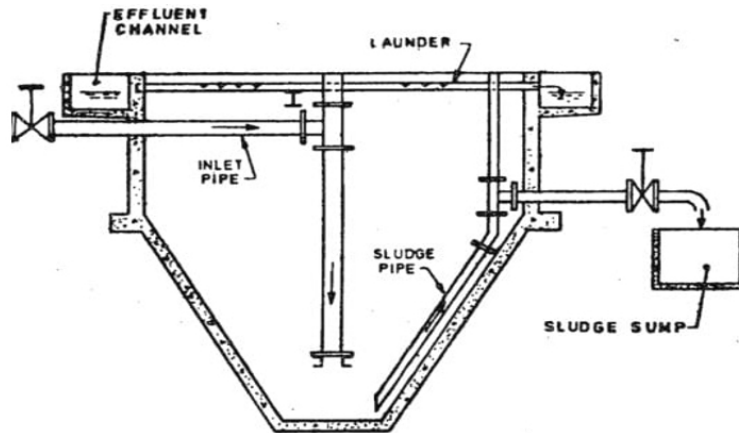


Fig. 9: Secondary Sedimentation Tank<sup>8</sup>

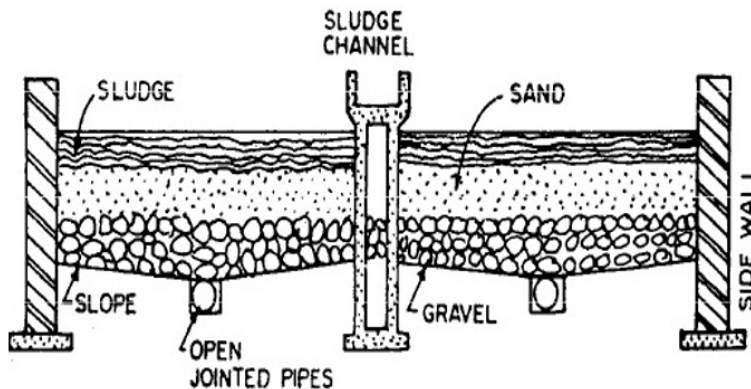


Fig. 10: Sludge drying beds<sup>8</sup>

digested sludge before it disposed of or dump somewhere.

Volume of sludge = Quantity sewage / Sludge applied  
X Specific gravity X Solid content (4)

Volume of sludge per cycle = Volume of sludge X  
Period of each cycle

Area of bed required =  $\frac{\text{Volume of sludge per cycle} (4)}{0.3}$

### Results

According to the survey, the population of the JAU campus is 1418 persons in the year 2012, and it is expected to 1888 persons in the year 2042 as per assumed 10% incremental growth. It is found that the domestic water supply within JAU campus is about 0.432 MLD as per study of water supply survey. It is also worked out in sewage water survey that sewage flow rate is 0.0084m<sup>3</sup>/s; which is very low sewage discharge. The care has been taken in the said design of STP to fulfill the requirement of standard design, but looking to the discharge and quality of sewage water the designed plant is not economically feasible, so it is suggested that the additional sewage water should be channelized to the a fore said STP, to have cost-effectiveness and efficiency of plant.

To handle this low discharge, one circular collecting chamber is designed admeasuring 14m diameter and 2.50 m. deep, which collects the sewage water throughout the day and collected sewage water discharged to said STP, by means of this collecting

chamber the discharge to STP can be maintained. So it is required that, the plant run in two shift for 1.5 hours which results in 0.0672 m<sup>3</sup>/s discharge within STP.

### Conclusion

Wastewater treatment includes a variety of processes performed at different levels of treatment. The essential type of treatment is the separating of natural waste by microscopic organisms either vigorously or anaerobically or a mix of both which happens in optional treatment. Essential treatment offers the settlement of solids. Tertiary treatment includes the evacuation of phosphorus, nitrogen and toxic substances. Pathogen expulsion happens all through treatment yet turns out to be more compelling for the most part at tertiary levels using UV beams and chlorination. The higher the treatment productivity the better quality of effluent produced.

- As per design point of view first, construct sewage collating at Hostel area and staff residential area which convey wastewater to STP timely and efficiently and also provide to a facility of repair and maintenance and also keep in mind future expansion.
- As per the design point of view, discharge is very low so, the plant cannot run 24-hr. Therefor STP run only 3-hr in a day and provide an extra construction of collating chamber.
- Running of more than 3-hr in a day for decrease operating cost and increase saving of electricity of pumping irrigation water.

Table 4: Design details

Component	TYPE	NOS	DIMENSIONS
Receiving chamber		1	14 m ØX 2.36 m (SWD) + 0.14m (FB)
Coarse screen	1 mechanical	1	0.51X 0.7m (SWD) + 0.3 m (FB)
Grit chamber	Horizontal Flow type	1	1.2m X 5m X 2.5m
Fine screen	Disc type, Mechanical	1	97 nos. of bar,3 mm thickness of bar, 0.3 m(SWD),0.58 m periphery of disc
Skimming tank	Air diffuser + Chlorine gas	1	25m X 0.90m X 2.5m + 0.5m (FB)
Secondary clarifier	Circular type, Radial flow	1	6m dia X 3.5m (SWD) + 0.5m (FB)
Sludge drying bed	Sand + Gravelled	2	1m X 1.25m



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